GREATER AUGUSTA UTILITY DISTRICT WASTEWATER TREATMENT FACILITY



WHO WE ARE

WASTEWATER TREATMENT PLANT STAFF: OPERATIONS, SAFETY AND LABORATORY

- OVER 100 COMBINED YEARS' EXPERIENCE
- DEDICATED TO PROTECTING THE ENVIRONMENT.
- CONTINUING EDUCATION VIA PROFESSIONAL ORGANIZATIONS AND IN-HOUSE TRAINING
- 3 MAINE DEP-CERTIFIED GRADE V-B WASTEWATER OPERATORS



WHY WE ARE HERE

- TO **REMOVE POLLUTANTS** FROM INCOMING WASTEWATER, 4 44 MGD
 - COMMERCIAL, RESIDENTIAL AND INDUSTRIAL SOURCES
 - RAIN FLOWS
 - SNOW MELT
- TO DISCHARGE TREATED, RECLAIMED WATER TO THE KENNEBEC RIVER



- ADMINISTERED BY THE MAINE DEPARTMENT OF ENVIRONMENTAL PROTECTION
- ALL DISCHARGES TO "WATERS OF THE STATE" MUST HAVE A PERMIT
- PERMIT LIMITS: BASED ON "CLASSIFICATION" OF RECEIVING WATER—





Class B

- DISSOLVED OXYGEN CONTENT NOT BE LESS THAN 7 PARTS PER MILLION
- SUITABLE AS A HABITAT FOR FISH AND OTHER AQUATIC LIFE. THE HABITAT MUST BE CHARACTERIZED AS UNIMPAIRED.
- ESCHERICHIA COLI BACTERIA MAY NOT EXCEED 236 PER 100 MILLILITERS.
- DISCHARGES TO CLASS B WATERS MAY NOT CAUSE ADVERSE IMPACT TO AQUATIC LIFE

GAUD MEPDES Permit – Effluent Limitations

GREATER AUGUSTA UD #ME0100013 #W-002695-5M-I-R PERMIT

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SPECIAL CONDITIONS

A. EFFLUENT LIMITATIONS AND MONITORING REQUIREMENTS

 The permittee is authorized to discharge secondary treated sanitary wastewater from Outfall #001A to the Kennebec River. Such discharges shall be limited and monitored by the permittee as specified below. The italicized numeric values bracketed in the tables below and in the text on subsequent pages are code numbers that Department personnel utilize to code the monthly Discharge Monitoring Reports (DMRs). Footnotes are found on Pages 9-14.

Effluent Characteristic			Discharge	Limitations			Minimum Monitor	ing Requirements
	Monthly Average as specified	Weekly Average as specified	Daily Maximum as specified	Monthly Average as specified	Weekly Average as specified	Daily Maximum as specified	Measurement Frequency as specified	Sample Type as specified
Flow [50050]	8.0 MGD _[03]		Report MGD				Continuous 199 991	Recorder (RC)
Carbonaceous Biochemical Oxygen Demand (CBOD ₅)	1,668 lbs / Day _[26]	2,668 lbs / Day _[26]	Report lbs / Day _[26]	25 mg/L [19]	40 mg/L [19]	45 mg/L [19]	5/Week 105.071	Composite [24]
CBOD ₅ % Removal (1)	3230	(0.00		85% [23]			1/Month [01/30]	Calculate [CA]
Total Suspended Solids (TSS) [00530]	2,002 lbs / Day _[26]	3,002 lbs / Day _[26]	Report Ibs / Day _[26]	30 mg/L [19]	45 mg/L γ ₁₉₁	50 mg/L [19]	5/Week [05 07]	Composite [24]
TSS % Removal (1) [810]0]				85% [23]			1/Month [0] 30]	Calculate /CA/
Settleable Solids [00545]					***	0.3 ml/L (25)	1/Day [01.01]	Grab IGRI
E. coli Bacteria (2) From effective date until May 14, 2010 [3][633]	272 0	3 1111		142/100 mI ⁽³⁾	5-5:	949/100 ml	3/Week [03:07]	Grab _[GR]
E. coli Bacteria (2) Beginning May 15, 2010			THE	64/100 ml ⁽³⁾	(444)	427/100 ml	3/Week 103 071	Grab _[GR]
Total Residual Chlorine ⁽⁴⁾ From effective date until May 14, 2010 [50060]	***					1.0 mg/L [19]	2/Day [02 01]	Grab _[GR]
Total Residual Chlorine ⁽⁴⁾ Beginning May 15, 2010			202	(***)		0.82 mg/L	2/Day [02 01]	Grab _[GR]
Total Phosphorus 1006651 From June I – September 30	Report lbs / Day 1261		Report lbs / Day 1261	Report mg/L	(4)	Report mg/L	1/Month _[0] 30]	Composite [24]
pH (Std. Units) 1004001	***					6.0-9.0 //2/	1/Day [0] [0]	Grab (GRI
Arsenic (total) (5) [01002] (Upon permit issuance)	report lb/day [26]			report ug/L			1/Year [02/YR]	24-Hr. Composite
Arsenic (Inorganic) (6) 1012321 (Upon EPA test method approval)	0.27 lb / day [26]			4.1 ug/L [28]			1/Year [01/YR]	24-Hr. Composite









Rain Events/Snow Melt



Industrial



TO HEADWORKS



WEST SIDE INTERCEPTOR

WEST SIDE CONSOLIDATED CONDUIT

THE WASTEWATER TREATMENT PROCESS: PRELIMINARY TREATMENT

Incoming
Wastewater
("Influent")

New Bar Screen: Optimizes removal of sticks, rags, plastics, etc. ("Screenings"). Flow goes through grit chamber to FDS #1.



Bar Screen

THE WASTEWATER TREATMENT PROCESS: PRIMARY TREATMENT

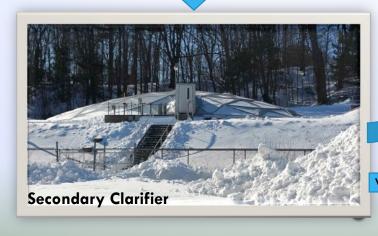
Primary
Treatment:
Removal of
floating
("scum") and
heavy solids
("Primary
Solids"). Liquid
goes to Flow
Distribution
Structure #2.



THE WASTEWATER TREATMENT PROCESS: SECONDARY TREATMENT

Secondary Treatment: Removal of dissolved and suspended solids ("Secondary Solids") via bacterial activity ("Activated Sludge"). Requires Pure Oxygen. Liquid from Aeration Tank goes to Secondary Clarifier.





Return Activated Sludge

Sludge Holding Tank

Primary + Secondary Solids

Waste Activated Sludge

PRIMARY + SECONDARY SOLIDS = BIOSOLIDS COMPOSTING: BENEFICIAL REUSE

- DEWATERED BIOSOLIDS ARE HAULED TO A COMPOSTING FACILITY
- COMPOSTING: "PROCESS TO FURTHER REDUCE PATHOGENS"
- THE DRIER THE SOLIDS, THE LOWER THE HAULING FEES
- 2015 BUDGET: \$347,200 (REVISED \$295,850)
- PROJECTED 2015 SAVINGS \$51,000
- 2015 JAN MAR = \$73,741 (\$81.98/TON)
- 2015 APRIL DEC = \$222,108 (74.11/TON)
- PROJECTED BUDGET FOR 2016 \$288,000
- \$72.00/TON 2016



DEWATERING PROCESS

TO REDUCE COST:

- THICKEN WASTE ACTIVATED SLUDGE BEFORE IT GOES TO SLUDGE HOLDING TANK TO REDUCE WATER CONTENT
- OPTIMIZE POLYMER SYSTEM TO ACHIEVE BEST SLUDGE FLOC
- ASSIGN PERSONNEL TO RUN PROCESS EFFICIENTLY
 - THIS HAS HELPED REDUCE POLYMER USE BY 4000 LBS/YR SAVING \$10,000

Floc with Polymer

 INSTALLED CHOPPER PUMP FOR SLUDGE HOLDING TANK TO MIX AND BLEND PRIMARY AND THICKENED SLUDGE TO PRODUCE A BETTER BELT FILTER PRESS FEED SLUDGE.





Sludge Holding Tank #1







3411 gallons/yr \$8,000 Sodium Hydroxide 27,052 gallons/yr \$27,000 (dependent on flow) Sodium Hypochlorite Sodium Bisulfite 5993 gallons/yr \$19,000 (dependent on flow) \$11,000 Liquid Oxygen 8400 gallons/yr 24 drums \$8,000 Defoamer \$21,000 Polymer 11,700 pounds

Total Chemical Budget 2015 - \$106,000

THE WASTEWATER TREATMENT PROCESS: EFFLUENT DISINFECTION — CHLORINATION AND DECHLORINATION

Disinfection:
Reduction of
diseasecausing
bacteria
("pathogens")



SECONDARY BYPASS (BYPASS OF THE SECONDARY WASTEWATER TREATMENT PROCESS)

High-Rate Disinfection Tank

- TRIGGER:
 - INSTANTANEOUS FLOWS > 12 MILLION GALLONS PER DAY
- GOES THROUGH PRIMARY TREATMENT
- BYPASSES SECONDARY TREATMENT PROCESS
- DISINFECTION IN HIGH-RATE DISINFECTION TANK
- DECHLORINATION IN HIGH-RATE DISINFECTION TANK



GAUD MEPDES Permit – Secondary Bypass Effluent Limitations

GREATER AUGUSTA UD #ME0100013 #W-002695-5M-I-R PERMIT

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SPECIAL CONDITIONS

A. EFFLUENT LIMITATIONS AND MONITORING REQUIREMENTS (cont'd)

3. The permittee is authorized to bypass secondary treatment, identified herein as Outfall #001B (internal waste-stream). Such CSO related discharges may only occur in response to wet weather events when the influent to the wastewater treatment facility exceeds an instantaneous flow rate of 8,333 gallons per minute (12.0 MGD) or in accordance with the most current approved Wet Weather Flow Management Plan. Discharges shall be monitored and reported as specified below. Approval of said bypass will be reviewed and may be modified or terminated pursuant to Special Condition Q, Reopening of Permit for Modification, if there is substantial change in the volume or character of pollutants in the collection/treatment system.

Effluent Characteristic		Discharge	Minimum Monitoring Requirements			
	Monthly <u>Average</u> as specified	Daily <u>Maximum</u> as specified	Monthly Average as specified	Daily Maximum as specified	Measurement Frequency as specified	Sample Type as specified
Flow, MGD [50050]	Report Total MGD 1031	Report MGD 1031			Continuous	Recorder
Surface Loading Rate ⁽¹⁰⁾ /50050/		Report gpd/sf [07]	***		1/Discharge Day(11)	Calculate (CA)
Overflow Use, Occurrences ⁽¹²⁾			Report # of days		1/Discharge Day ⁽¹⁾	Record Total
CBOD ₅ From effective date until March 31, 2009 80082	(444)	***	1231	Report mg/L [19]	1/Discharge Day(11)	Composite [24]
CBOD ₅ % Removal ⁽¹³⁾ From effective date until Mar. 31, 2009 [810]01			Report (%) [23]		1/Discharge Day(11)	Calculate [24]
BOD ₅ Beginning April 1, 2009				Report mg/L [19]	1/Discharge Day(11)	Composite [24]
BOD ₅ % Removal ⁽¹³⁾ Beginning April 1, 2009 [8]0[0]		***	Report (%) /23/	***	1/Discharge Day(11)	Calculate [24]
TSS [00530]				Report mg/L /19/	1/Discharge Day ⁽¹¹⁾	Composite [24]
TSS % Removal ⁽¹³⁾ [81011]			Report (%) [23]		1/Discharge Day(11)	Calculate [24]
E. coli Bacteria (2) From effective date until May 14, 2011 [31633]				949/100 ml	1/Discharge Day ⁽¹¹⁾	Grab
E. coli Bacteria (2) Beginning May 15, 2011 [31633]			70 10 AF	427/100 ml _[13]	1/Discharge Day(11)	Grab _[GR]
Total Residual Chlorine ⁽⁴⁾ From effective date until May 14, 2011	7444			1.0 mg/L [19]	1/Discharge Day ⁽¹¹⁾	Grab





WE CAN'T "SET IT AND FORGET IT"

PROCESS CONTROL IS ESSENTIAL

- INFLUENT FLOW CHARACTERISTICS CHANGE CONSTANTLY DEPENDING ON MANY FACTORS SUCH AS RAIN, SPILLS, INDUSTRIAL AND DOMESTIC DISCHARGES. THROUGH PROCESS CONTROL PERSONNEL TRACK THESE TRENDS AND ADJUST PROCESS CONTROL PARAMETERS.
- SAMPLING/TESTING THROUGHOUT WASTEWATER TREATMENT TRAIN
- MICROSCOPIC EXAMINATIONS
- VISUAL OBSERVATIONS (COLORS, ODORS, FOAM)
- OPERATOR EXPERIENCE









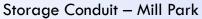
CSO ABATEMENT

PROJECTS

- PHASE I -1996 CSO ABATEMENT AND DEWATERING IMPROVEMENTS \$ 9,200,000
- PHASE II 2001 WEST SIDE CONSOLIDATED CONDUIT \$10,750,000
- PHASE III 2011 BOND BROOK COLLECTION SYSTEM \$18,130,000
 - BOND BROOK INTERCEPTOR \$14,520,000
 - CSO A1 AND A2 \$1,610,000
 - CSO III ENGINEERING \$2,000,000

Box Conduit

TOTAL COST OF CSO ABATEMENT TO DATE: \$44,046,539





\$ WWTP COST-SAVING INITIATIVES \$

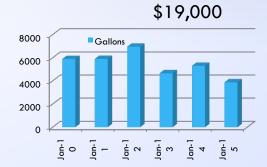
ITEM	INITIATIVE	SAVINGS

MOD RATE REDUCTION FROM 1.24 → 1.03 \$15,000

LEADER PROGRAM SCORE EXCELLENT \$6,000

SCHEDULE CHANGE REDUCED OVERTIME

HEATING FUEL REDUCED USE



BIOSOLIDS REDUCED COST/TON \$40,000

(BUDGET REDUCTION)

20

• TWO NEW ACRISON 515 POLYMER SYSTEMS -

COST \$96,506 (\$24,016 FOR LABOR AND \$72,490 FOR EQUIPMENT)

NEW SYSTEMS REDUCED POLYMER USE BY 1.6 LBS / BATCH SAVING \$8,000/YR

Old Acrison 500 Polymer Systems



New Acrison 515 Polymer Systems





TWO NEW 150 HP ATLAS COPCO COMPRESSORS FOR THE PRESSURE SWING ABSORBTION (PSA) SYSTEM

COST \$256,500 (\$221,084 FOR EQUIPMENT AND \$ 35,416 FOR LABOR)

REDUCED HP FROM 250 TO 150

Original 250 HP Compressor



150 HP Atlas Copco Compressors



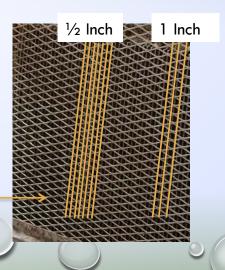
REDUCED BAR RACK BAR WIDTH FROM 1 INCH TO 1/2 INCH -

COST \$72,162

- THIS WILL REDUCE THE AMOUNT OF DEBRIS ALLOWED TO PASS THROUGH
 - REDUCES DAMAGE TO EQUIPMENT DOWN STREAM
 - REDUCES MAINTENANCE COST



Bars





INSTALLED 6 NEW BULK STORAGE CHEMICAL TANKS

COST \$126,636 (\$50,165 FOR EQUIPMENT, \$ 37,616 FOR LABOR AND \$38,855 FOR THE PIPING CHANGE ORDER)

 PROVIDES MORE STORAGE FOR CHEMICALS NEEDED FOR HIGH FLOW EVENTS AND REPLACE 34 OLD TANKS AND PIPING







INSTALLED ROTARY LOBE WASTE ACTIVATED SLUDGE PUMPS AND REMOVE 2 PENN VALLEY GRAVITY BELT THICKENER (GBT) PUMPS

COST \$27,658

- INSTALLED LARGER WASTE ACTIVATED SLUDGE PUMPS WITH THE CAPACITY TO PUMP TO THE GRAVITY BELT THICKENER SO 4-34 YR OLD PUMPS COULD BE REMOVED
- REDUCES COST BY SAVING ON MAINTENANCE, POWER AND EVENTUAL REPLACEMENT



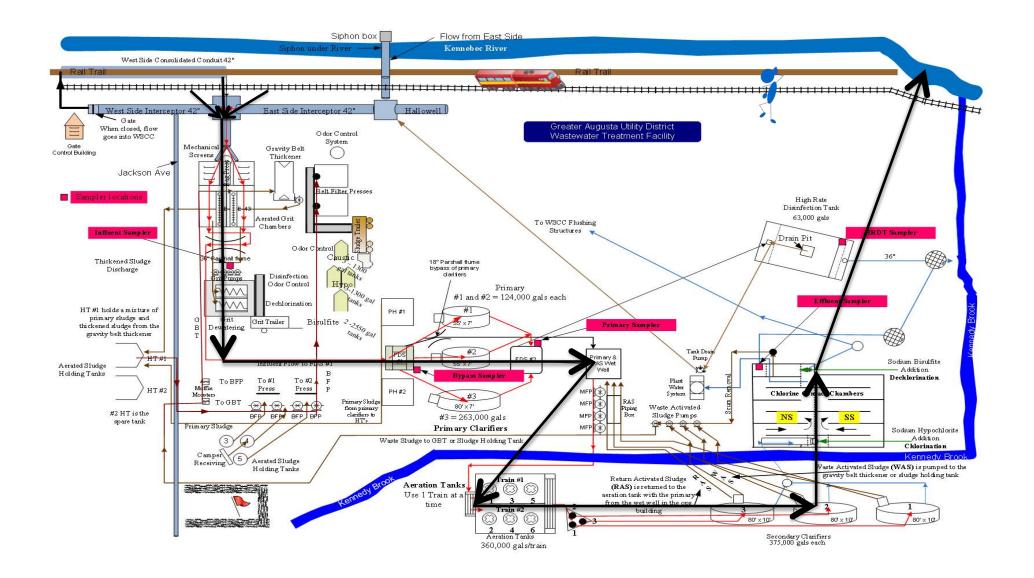
Gravity Belt Thickener (GBT) Pumps

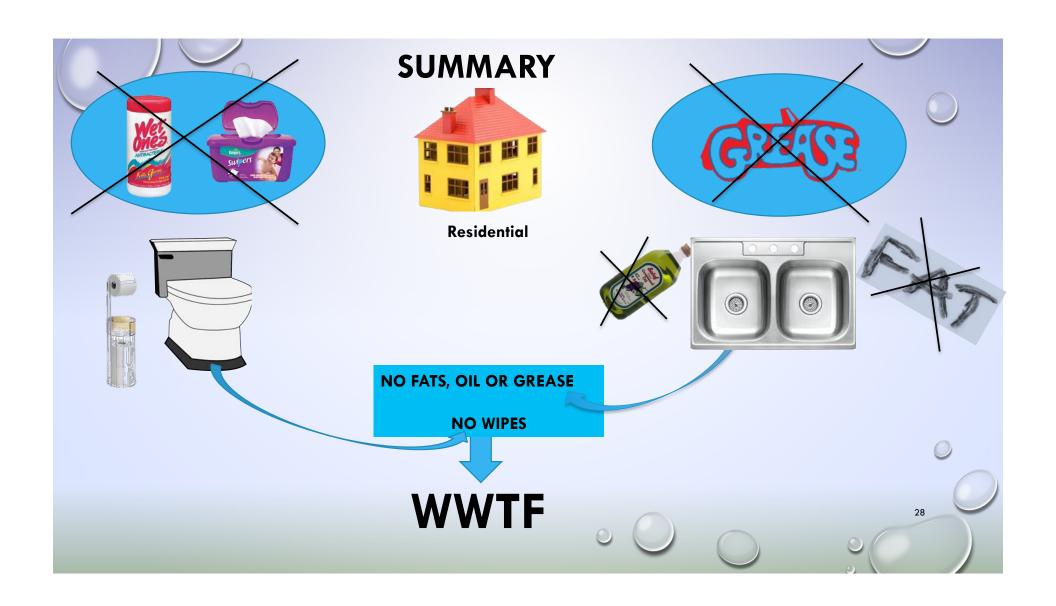




SUMMARY OF 2014 PROJECTS

- TOTAL COST OF 2014 WWTF PROJECTS: \$563,310
- STAFF ORDERED ALL EQUIPMENT TO SAVE ON CONTRACTOR MARK-UP
- ALL METAL FROM THE CONSTRUCTION WAS RECYCLED
- SUPPLIER SUBMITTED AN APPLICATION FOR AN EFFICIENCY MAINE GRANT FOR COMPRESSORS
- REPLACED 34-YEAR-OLD EQUIPMENT
- NEW EQUIPMENT SHOULD HAVE A 20-YEAR SERVICE LIFE





DISCHARGE OF TREATED WATER TO THE KENNEBEC RIVER











